

**5E6201**

Roll No. \_\_\_\_\_

Total No of Pages: **4****5E6201****B. Tech. V Sem. (Main/Back) Exam., Nov.-Dec.-2016****Mechanical Engineering****5ME1A Heat Transfer****Common with AE****Time: 3 Hours****Maximum Marks: 80****Min. Passing Marks Main: 26****Min. Passing Marks Back: 24***Instructions to Candidates:*

*Attempt any **five questions**, selecting **one question** from **each unit**. All questions carry **equal marks**. Schematic diagrams must be shown wherever necessary. Any data you feel missing suitably be assumed and stated clearly.*

*Units of quantities used/calculated must be stated clearly.*

*Use of following supporting material is permitted during examination.*

*(Mentioned in form No. 205)*

1. NIL \_\_\_\_\_2. NIL \_\_\_\_\_**UNIT - I**

Q.1 (a) Write the rate equations for the three modes of heat transfer. Define the symbols used and give the units for each. [8]

(b) Define and distinguish.

(i) Steady state.

(ii) Unsteady state and.

(iii) Transit state of heat transfer. [8]

**OR**

- Q.1 Explain the concept of thermal contact resistance. A furnace wall consists of an inside layer of silica brick 10cm thick ( $k=1.5 \text{ kcal/m-hr}^\circ\text{C}$ ) followed by a 20 cm layer of magnesite brick ( $k=5 \text{ kcal/m hr}^\circ\text{C}$ ) on the outside. The inside surface of the silica brick wall is maintained at  $750^\circ\text{C}$  whilst the outside surface of magnesite is at  $125^\circ\text{C}$ . The contact thermal resistance between the two walls at the interface is  $0.003 \text{ hr}^\circ\text{C /kcal}$  per unit wall area. What is the rate of heat loss per unit area of the wall? Also calculate the temperature drop at the interface. rtuonline.com [16]

**UNIT – II**

- Q.2 (a) Define fin efficiency. In which medium (gas or liquid) will the use of fins be more effective and why? [8]
- (b) A long aluminum cylinder of radius 10 cm which is initially at a uniform temperature of  $350^\circ\text{C}$  is suddenly exposed to an environment at  $30^\circ\text{C}$ . The convection heat transfer coefficient between the cylinder's surface and the environment is  $1000 \text{ W/m}^2\text{k}$ . Determine the time required for the axis of the cylinder to attain a temperature of  $126^\circ\text{C}$ . [8]

**OR**

- Q.2 Derive the energy equation for the laminar boundary layer on a flat plate. Explain its importance in heat transfer. [16]

### UNIT – III

- Q.3 A plate heater  $0.4 \times 0.4$  m using electrical elements, has a constant heat flux of  $1.2 \text{ kW/m}^2$ . It is placed in room air at  $20^\circ\text{C}$  with the hot side facing up. Determine the value of  $h$  and average plate temperature. [16]

#### OR

- Q.3 (a) With a sketch of boiling curve explain the type of flow regimes. [8]  
(b) Steam at  $65^\circ\text{C}$  condenses on vertical tube of diameter of  $0.3\text{m}$  at  $55^\circ\text{C}$ . Determine the location at which the film will become turbulent. [8]

### UNIT – IV

- Q.4 (a) Discuss the importance of heat exchangers for industrial use. Classify it with neat sketches. [8]  
(b) Differentiate the parallel and counter flow type heat exchangers. [8]

#### OR

- Q.4 A shell and tube oil to water heat exchanger has tubes of internal diameter  $12\text{mm}$  and length  $2\text{m}$  in a single shell. Cold water ( $C_{pc} = 4180 \text{ J/kg}^\circ\text{C}$ ) enters the tubes at  $33^\circ\text{C}$  with a flow rate of  $5 \text{ kg/s}$  and leaves at  $55^\circ\text{C}$ . Oil ( $C_{ph} = 2150 \text{ J/kg}^\circ\text{C}$ ) flows through the shell and is cooled from  $120^\circ\text{C}$  to  $75^\circ\text{C}$ . The overall heat transfer coefficient is  $U_i = 885 \text{ W/m}^2\text{ }^\circ\text{C}$  based on the internal area of the tubes. Determine the number of tubes required in this heat exchanger. [16]

### UNIT – V

Q.5 Two large parallel planar surfaces are maintained at 400 and 800k, respectively. The surfaces are non-gray and have the emissivity variation given below:-

Surface 1:

$$T_1 = 800\text{k}, E_{1,1} = 0.6 \text{ for } 0 < \lambda < 3 \mu\text{m}; E_{1,2} = 0.2 \text{ for } \lambda > 3 \mu\text{m}.$$

Surface 2:

$$T_2 = 400\text{k}, E_{2,1} = 0.2 \text{ for } 0 < \lambda < 3 \mu\text{m}; E_{2,2} = 0.6 \text{ for } \lambda > 3 \mu\text{m}.$$

Determine the heat transfer between the two planes per unit area using a non-gray analysis. Compare this with a gray analysis based on the equivalent gray emissivities of the two surfaces at their respective temperatures. [16]

OR

Q.5 Write short note on: [16]

- (a) Plank distribution law.
  - (b) Krichoff's law.
  - (c) Radiation intensity.
  - (d) Shape factor.
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